

# Role of Thermophysical Properties in Weld Pool Modeling

*The effects of variations in thermophysical properties in models on heat transfer and fluid flow is examined*

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**ABSTRACT.** The results of numerical simulation of heat transfer and fluid flow in the weld pool strongly depend on the physical processes considered and the input data used in the model. The aim of this paper is to examine the impact of the thermophysical properties on the results of such calculations. The effects of various thermophysical properties such as the viscosity, thermal diffusivities of both the solid and liquid, the temperature coefficient of surface tension and the energy absorption coefficient on the depth and the diameter of the weld pool, and the weld pool surface velocities and temperature distributions are analyzed. The relative importance of the various thermophysical properties are identified from the computed results.

## Introduction

The structure and properties of the welds are strongly affected by heat transfer and metal flow in the weld pool and alloying element loss from the weld surface. Although the diagnostic techniques for measuring pool temperatures are currently being evaluated and developed, direct reliable measurements of velocities, temperatures and species concentrations in the weld pool are extremely difficult since the weld pool is small in size and often covered by an intense plasma (Refs. 1–3). A recourse is to simulate the temperature and velocity fields

by mathematical modeling of the essential physical features of a welding process. For the prediction of the weld pool geometry, the temperature fields and the cooling rates, the traditional heat conduction models (Refs. 4–6) are being increasingly replaced by more accurate calculation procedures (Refs. 7–22), which take into account the weld pool convection due to the combined effects of the buoyancy, electromagnetic and the surface tension forces. Indeed, the modeling of heat transfer, fluid flow and mass transfer has already been successful in revealing detailed insight about various aspects of the welding process which could not have been obtained otherwise.

Despite the success of the modeling approach in welding, insufficient help is available to most beginner researchers to enable them to meaningfully apply this powerful tool to achieve trustworthy results in a realistic time frame. Currently, there are at least two main diffi-

culties in using mathematical modeling to solve welding problems. First, since the welding processes are more complicated than most other high-temperature thermochemical processes, practical simulation of heat and mass transfer and fluid flow in the weld pool mandates considerable simplification in the modeling efforts. A fully comprehensive modeling of weld pool heat transfer and fluid flow is computationally intensive. As a consequence, one is confronted with the precarious task of having to make some sort of judgment about what level of simplification is adequate for a particular application. In practice, this involves making a decision to choose, often without any objective basis, which physical processes are to be considered important and emphasized in the construction of the model and which others must be considered as less important details and, consequently, greatly simplified or even completely ignored in the mathematical framework. Recent welding simulation literature is a testimony of the large numbers of such choices. Three-dimensional vs. two-dimensional simulations, transient vs. steady state, flat weld pool surface vs. free deformable surface, laminar structure of flow in the weld pool vs. turbulent flow simulated using various turbulence models of different degrees of sophistication are all examples of the choices that must be consciously made prior to undertaking the numerical simulation. While it is expedient to weigh heavily in favor of a particular set of simplifications because of the availability of an existing software or other computational conveniences, the consequences of such choices vary depending upon the goals of the simulation effort.

## KEY WORDS

Weld Pool Modeling  
Thermophysical Prop.  
Numerical Simulation  
Heat Transfer  
Fluid Flow  
Viscosity  
Thermal Diffusivity  
Surface Tension  
Power Absorption  
Weld Pool Simulation

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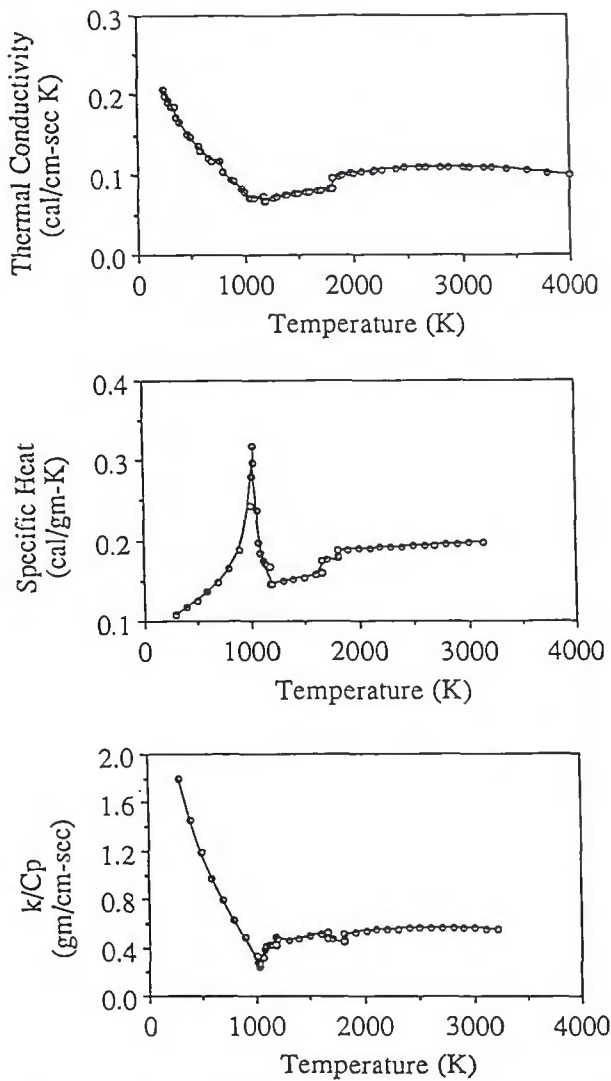


Fig. 1 — Variation of thermal conductivity,  $k$ , specific heat,  $C_p$ , and  $k/C_p$  as a function of temperature for iron.

sion,  $dy/dT$ , to calculate the shear stress at the weld pool surface. Thus, for a constant density and given laser beam power density distribution, the important properties required for the calculations are the absorption coefficient, the temperature coefficient of surface tension, viscosity of the molten metal, the ratio of thermal conductivity and the specific heat for both the solid and the liquid phases. The plots of specific heat,  $C_p$ , thermal conductivity,  $k$ , and their ratio,  $k/C_p$  for iron as functions of temperature are presented in Fig. 1. It is observed from Fig. 1 that for solid iron, the values of  $k/C_p$  vary from 0.24 gm/cm-s to 1.8 gm/cm-s. However, since temperature-independent constant values of  $k/C_p$  of solid are frequently used in the literature, it is important to understand the consequences of such practice.

Figure 2 shows the velocity and temperature fields for four different cases.

The enthalpies were converted to temperatures using data presented in Fig. 3. The values of the thermophysical properties used for the calculations are indicated in Table 1. It is observed from the computed results that depending on the values of the thermophysical properties used, the pool geometry, the temperature and the velocity fields can vary significantly.

In heat transfer and fluid flow calculations, enhanced values of viscosities are commonly used to simulate the effects of turbulence. Depending on the particular turbulence model adapted, the computed values of effective viscosity and its spatial distribution vary significantly. Furthermore, high values of viscosity are also utilized to achieve numerical stability in computations. In fact, for the welding of a given material, a wide range of viscosity values have been used by various investigators for weld

pool modeling. The computed values of width, depth and aspect ratio of the weld pool, the maximum velocity and peak temperature, and the Peclet number for heat transport are plotted as a function of viscosity in Fig. 4. The Peclet number is a measure of the relative magnitudes of convective and diffusive heat trans-

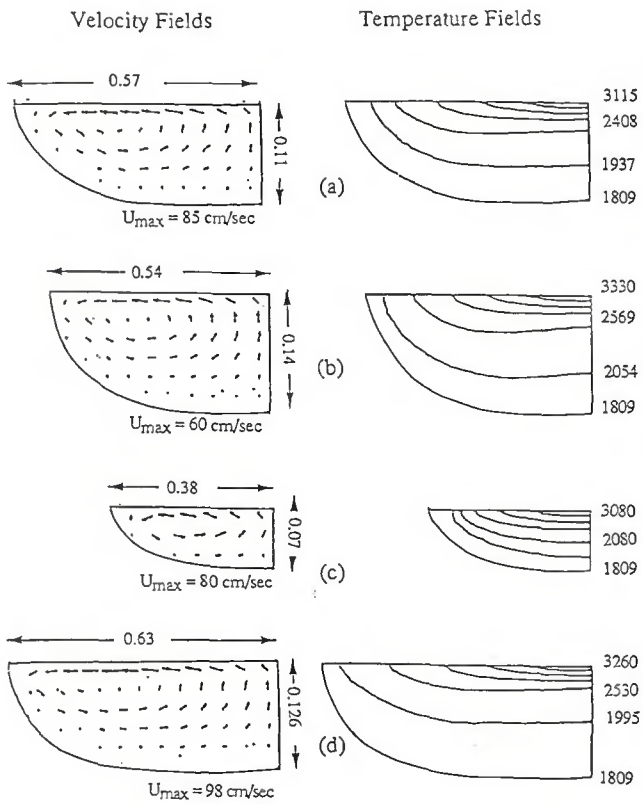


Fig. 2 — Velocity and temperature fields for four different cases. A — Data used from Table 1; B — viscosity used is 1.0 gm/cm-s; C —  $k/C_p$  of solid used is 0.48 gm/cm-s; D — absorption coefficient used is 0.18. All dimensions are in mm and temperatures in K.

Table 1—Data Used for Calculations

Property/Parameter	Value
Density (gm/cm <sup>3</sup> )	7.80
Melting Point (K)	1809.0
Laser Power (watts)	500.0
Radius of the Beam (cm)	0.02
Viscosity (gm/cm-s)	0.40
$k/C_p$ of Solid (gm/cm-s)	0.24
$k/C_p$ of Liquid (gm/cm-s)	0.54
Absorption Coefficient	0.15
Temperature Coefficient of Surface Tension (dyne/cm-s)	-0.50



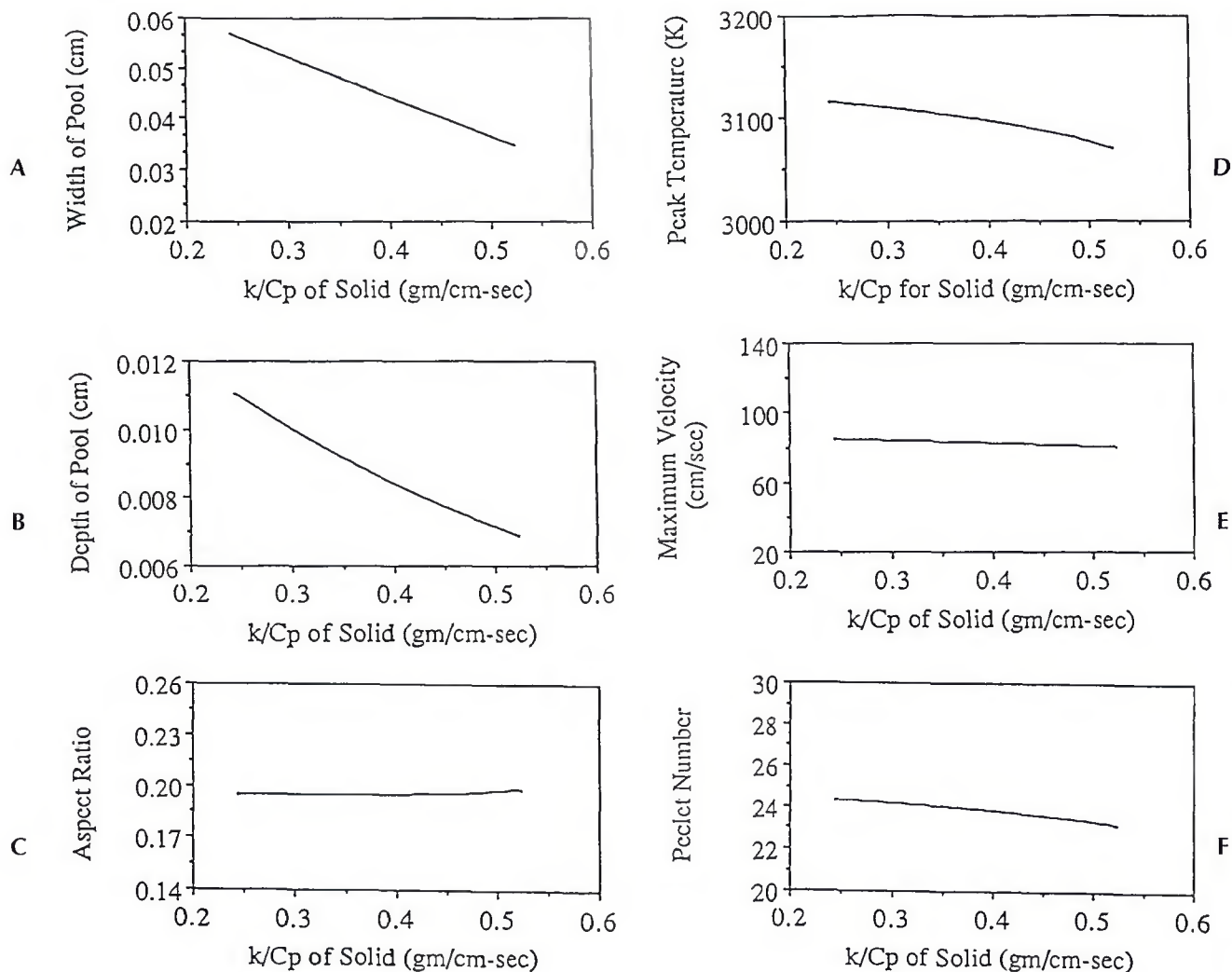


Fig. 5 — Effects of  $k/C_p$  of solid on: A — diameter; B — depth; C — aspect ratio of the weld pool; D — the peak temperature; E — maximum surface velocity; F — the Peclet number for heat transfer.

plies a major role of conduction heat transfer. For example, the use of an infinitely large viscosity amounts to solving heat conduction equation in the weld pool. Lancaster (Ref. 24) has demonstrated that the use of conduction models always results in high peak temperatures. When high values of viscosity are used, the weak surface velocities and negative value of the temperature dependence of surface tension lead to smaller width and larger depth of the weld pool and, consequently, higher depth-to-width ratio, commonly described as the aspect ratio. The variation in the viscosity from 0.1 to 1.0 gm/cm-s results in the increase in aspect ratio by 30%. However, it is to be pointed out here that the trends in the variation of the various simulated results will change when one considers positive temperature coefficient of surface tension. For example, when the temperature coefficient of surface tension is positive, an increase in the viscosity will result in a

decrease in radially inward-directed velocity, a decreased depth and increased width, and as a consequence, a decreased aspect ratio. However, since the purpose of the investigation is to bring out the sensitivity of the properties used on the calculated results, the trends in the variation of the results are explained only for the case when the temperature coefficient of surface tension is negative.

The spatial distribution of viscosity in strongly agitated turbulent systems is computed using an appropriate turbulence model. The currently available turbulence models were formulated to deal with mainly parabolic flows in large systems where the physical dimensions were much larger than the width of the weld pool. In laser melted weld pools, the dimensions are often of the order of millimeters and the velocities can reach up to about a meter a second. The occurrence of large recirculating velocities in a small region in the weld pool

makes the structure of the flow in laser melted weld pools very different from the flow structure encountered in most other materials processing systems. The validity of the currently available turbulence models for the modeling of the weld pool is therefore open to question. Thus, in the absence of adequate knowledge about the structure of fluid flow in weld pools, the values of viscosity are currently prescribed somewhat arbitrarily.

Thermal diffusivity of solid is an important thermophysical property which influences the geometry of the weld pool. In the literature, widely different values of  $k/C_p$  of solid have been used for the same material. The effects of  $k/C_p$  on the weld pool geometry, peak temperature and the maximum surface velocity are presented in Fig. 5. Both the width and the depth of the pool decrease with an increase in the  $k/C_p$  value. For example, when the value of  $k/C_p$  is increased from 0.24 to 0.52 gm/cm-s, both







