

clarifies the mathematical relation between the two indexes.

Heat Flow of Ideal Quench

If the temperature of a liquid medium used to quench a cylindrical bar is assumed to be zero, the heat conduction equation for two-dimensional cylindrical coordinates (Fig. 1) is

$$\frac{\partial \theta}{\partial t} = \kappa \left(\frac{\partial^2 \theta}{\partial r^2} + \frac{1}{r} \frac{\partial \theta}{\partial r} \right) \quad (8)$$

where κ = thermal diffusivity, θ = temperature, and t = time.

Because of its symmetry with respect to angle ψ , temperature θ is a function of radius r and time t alone. When a bar is heated up to θ_p before quench, then the initial condition is

$$\theta = \theta_p, \quad 0 \leq r \leq a \quad (t=0) \quad (9)$$

If a cylindrical bar is ideally quenched, the surface temperature of the bar instantly becomes zero. Hence, the boundary condition becomes

$$\theta = 0, \quad r = a \quad (10)$$

The solution that satisfies Equations 8, 9 and 10 is given as follows:

$$\theta = 2\theta_p \sum_{n=1}^{\infty} \frac{1}{j_n} \cdot \frac{J_0\left(j_n \frac{r}{a}\right)}{J_1(j_n)} \exp\left(-j_n^2 \kappa \frac{t}{a^2}\right) \quad (11)$$

where, j_n is a n -th root of the following Eigen value equation:

$$J_0(x) = 0, \quad J_0 \text{ is 0-order Bessel function} \quad (12)$$

At the center ($r = 0$), Equation 11 becomes

$$\theta = 2\theta_p \sum_{n=1}^{\infty} \frac{1}{j_n} \cdot \frac{1}{J_1(j_n)} \exp\left(-j_n^2 \kappa \frac{t}{a^2}\right) \quad (13)$$

where J_1 is a first-order Bessel function. By substituting 800° and 500°C into θ in Equation 13, respectively, cooling times to 800°C, t_{800} , and to 500°C, t_{500} , from θ_p at the center of a quenched bar can be calculated.

A study is presently being conducted for cases in which a full martensite or a 50% martensite is obtained at the center of cylindrical bar specimens. Hence,

$$a = \frac{D_I}{2} \quad (14)$$

Table 1 — Carbon Coefficients in the Taylor Series

$B_C^{(a)}$	CE_{HARDEN}	CE_{HARDEN}	Ref. 4
8.3	10.6	8.4	9.8

(a) Calculated by Equation 26.

Meanwhile, the logarithm of $t_{8/5}$ is:

$$\ln(t_{8/5}) = \ln(t_{500} - t_{800}) \quad (15)$$

$t_{8/5}$ in Equation 15 becomes T_M only when the radius of a quenched bar is half of the ideal diameter (Equation 14). In this case, $t_{8/5}$ is the longest cooling time to obtain full martensite. The empirical relation of Equation 3 implies that $\ln(T_M)$ is a function of many variables (C, Si, Mn, P, S , etc.). Hence, $\ln(T_M)$ can be expressed in the manner of the Taylor series. The Taylor series of a multi-variable function is given as follows:

$$\begin{aligned} f(x_1, x_2, \dots, x_n) &= f(a_1, a_2, \dots, a_n) + (x_1 - a_1) \\ &\frac{\partial f(a_1, a_2, \dots, a_n)}{\partial x_1} + (x_2 - a_2) \frac{\partial f(a_1, a_2, \dots, a_n)}{\partial x_2} \\ &+ (x_n - a_n) \frac{\partial f(a_1, a_2, \dots, a_n)}{\partial x_n} + \sum_{m=2}^{\infty} \frac{1}{m!} \\ &\left((x_1 - a_1) \frac{\partial}{\partial x_1} + (x_2 - a_2) \frac{\partial}{\partial x_2} \right. \\ &\left. + (x_n - a_n) \frac{\partial}{\partial x_n} \right)^m f(a_1, a_2, \dots, a_n) \quad (16) \end{aligned}$$

When $\ln(t_{8/5})$ in Equation 15 is expressed in the Taylor series, the second and higher order terms and cross-terms from Equations 3 and 4 can be neglected. Therefore,

$$\begin{aligned} \ln(T_M[C, Si, Mn, \dots]) &= \ln(T_M[C_0, Si_0, Mn_0, \dots]) + B_C(C - C_0) \\ &+ B_{Si}(Si - Si_0) + B_{Mn}(Mn - Mn_0) + \dots \quad (17) \end{aligned}$$

where, B_X (e.g., $B_C, B_{Si}, B_{Mn}, \dots$) is a first-order coefficient of element X (e.g., C, Si, Mn, \dots).

$$B_x = \frac{\partial \ln(T_M)}{\partial x} \Big|_{C=C_0, Si=Si_0, Mn=Mn_0, \dots} \quad (18)$$

The following correlation between the critical cooling time and critical diameter is given in Appendix A:

$$\frac{\partial \ln(T_M)}{\partial x} = 2 \frac{\partial \ln(D_I)}{\partial x} \quad (19)$$

From Equations 18 and 19, the following relation is obtained:

$$2 \frac{\partial \ln(D_I)}{\partial x} = B_x \quad (20)$$

Integration of Equation 20 with respect to X gives

$$\ln(D_I) = \frac{B_x}{2} X + G \quad (21)$$

where, G is a function of elements other than X .

Equation 20 is valid for any element, therefore

$$\ln(D_I) = B_0 + \frac{B_C}{2} C + \frac{B_{Si}}{2} Si + \frac{B_{Mn}}{2} Mn + \dots \quad (22)$$

where, B_0 is a constant.

From Equation 22,

$$\begin{aligned} D_I &= \exp(B_0) \cdot \exp\left(\frac{B_C}{2} C\right) \cdot \exp\left(\frac{B_{Si}}{2} Si\right) \\ &\cdot \exp\left(\frac{B_{Mn}}{2} Mn\right) \cdot \dots = D_{I0} f_C f_{Si} f_{Mn} \dots \quad (23) \end{aligned}$$

where $D_{I0} = \exp(B_0)$, $f_C = \exp\left(\frac{B_C}{2} C\right)$, \dots

Equation 23 is virtually equal to the multiplying factor of Equation 6. Equation 23 has been derived from the condition that $\ln(T_M)$ is expressed as a linear combination of the concentration of each alloy, i.e., carbon equivalent. Hence, it is concluded that D_I should be expressed by multiplying factors as long as the carbon equivalent is expressed as a linear combination of each element. Furthermore, the critical cooling time T_M is given from Equation 17,

$$\ln(T_M) = B_0' + B_C \left\{ C + \left(\frac{B_{Si}}{B_C}\right) Si \right. \\ \left. + \left(\frac{B_{Mn}}{B_C}\right) Mn + \dots \right\}$$

where $B_0' = \ln(T_M[C_0, Si_0, Mn_0, \dots])$

$$- (B_C C_0 + B_{Si} Si_0 + B_{Mn} Mn_0 + \dots) \quad (24)$$

The second term in the right side in Equation 24, $\{C + (B_{Si}/B_C)Si + (B_{Mn}/B_C)Mn + \dots\}$, is considered to be the carbon

Table 2 — Multiplying Factors of Alloy Elements

Element	Ref. 19	Ref. 20	Ref. 21 ^(a)	Ref. 22 ^(a)	Ref. 23 ^(a)
Si	1+0.64Si	1+0.67Si	1+0.55Si	1+1.25Si	1+0.85Si
Mn	1+4.1Mn	1+4.8Mn	1+1.2Mn	—	1+3.3Mn
Cr	1+2.33Cr	1+2.16Cr	1+1.73Cr	—	1+2.3Cr
Ni	1+0.52Ni	1+0.74Ni	1+0.42Ni	1+0.3Ni	1+0.36Ni
Mo	1+3.14Mo	1+2.53Mo	1+1.78Mo	1+5.0Mo	1+3.2Mo
Cu	1+0.27Cu	—	1+0.45Cu	—	—

(a) Determined by the authors using the graphic data.

