

If k or c are functions of T , Equation 1 is nonlinear. On the boundary of Ω , either the essential or natural boundary condition must be satisfied. The essential boundary condition can be defined as

$$T(x,y,z,t) = T(x,y,z,t) \quad \text{on the boundary } S_1; \quad \text{i.e., } (x,y,z) \in S_1; t > 0 \quad (2)$$

The natural boundary condition can be defined as

$$k_n \frac{\partial T}{\partial n} + q + h(T - T_o) + \sigma \epsilon (T^4 - T_o^4) = 0 \quad (3)$$

on the boundary S_2 ; i.e., $(x,y,z) \in S_2; t > 0$.

- $q(x,y,z,t) =$ a prescribed flux (W/m^3)
- $k_n =$ thermal conductivity normal to the surface ($W/m C$)
- $h =$ heat transfer coefficient for convection ($W/m^3 C$)
- $T_o =$ ambient temperature for convection and/or radiation (C)
- $G =$ Stefan-Boltzmann constant $\epsilon = (W/m^2 C^4) =$ emissivity (the full amount of energy emitted per m^2 of a black body/h)

If radiation is included or if the convective heat transfer coefficient is temperature dependent this boundary condition is nonlinear. In addition, the initial condition must be specified for $(x,y,z) \in \Omega$

$$T(x,y,z,0) = T_o(x,y,z) \quad (4)$$

If the partial differential Equation 1, the boundary conditions of Equations 2 and 3, and the initial condition of Equation 4 are consistent, the problem is well posed and a unique solution exists. The FEM imposes a piece-wise polynomial approximation of the temperature field within each element

$$T(x,y,z,t) = \sum_{i=1}^n N_i(x,y,z) T_i(t) \quad (5)$$

where
 $n =$ the number of nodes
 $N =$ basis functions dependent only on the type of element and its size and shape

Decoupling the Heat Equation

Whether or not the heat equation is coupled to other equations such as the Navier-Stokes or MHD equations, the temperature field belongs to the Sobolev space, H_0^1 . In simplistic terms, the energy and the flow of energy must be finite as expressed by the following equations:

$$\int_{\Omega} T^2 d\Omega < \infty \quad \text{and} \quad \int_{\Omega} \nabla T^2 d\Omega < \infty \quad (6)$$

If the temperature field belongs to H_0^1 , the FEM solution to the uncoupled heat equation always exists regardless of whether the heat equation is coupled or not. More precisely, functions Q and q that generate a temperature field by the heat equation always exist. It is equally true that with any temperature field if H_0^1 is prescribed, the heat equation will generate unique functions Q and q .

Therefore, in order to decouple the heat equation, it is necessary to find the Q and q functions that generate the desired temperature field. In welding, functions Q and q represent the heating effect of the arc called heat source models. In solving the uncoupled heat equation, these functions account for heat transfer effects such as the heat transported by moving liquids and/or resistive heating, I^2R .

The main thrust of this paper is to show that the 2D approximation requires a different Q from the 3D discretization to account for the lack of diffusive heat transfer in the longitudinal direction.

Model for Welding Heat Sources

For welding situations where the effective depth of penetration is small and the bead symmetric, the Pavelic, Friedmann and Krutz models have been quite successful (Refs. 8–11). However, for high power density sources such as a laser or electron beam and most arcs, flux models ignore the digging action of the arc or beam that transports heat well below the surfaces and does not predict the correct weld nugget shape. In such cases a PDDF is preferred. These are called flux or PDDF heat source models. The following physical and mathematical interpretation of the flux and PDDF heat source models is now proposed.

Assume the exact temperature is known and prescribed in Equation 1. The applied flux boundary condition can be evaluated as a Lagrange multiplier. The PDDF can be evaluated as the residual in Equation 1. Of course, in the most important case, $T(x,y,z,t)$ is sought and the flux and/or PDDF must be specified as data. Nevertheless, this interpretation will be shown to lead to useful results.

Kinematic models: to reduce computing costs of solving a full 3D heat equation, Equation 1 was simplified by assuming some terms were zero. The most popular assumption is that $\partial T / \partial z = 0$ where z is the longitudinal direction. This leads to a surprisingly subtle cross-sectional model. It is equivalent to a 3D steady state solution with the added constraint that $\partial T / \partial z = 0$. This paper is concerned primarily with the error introduced by this constraint. The double

ellipsoidal PDDF proposed by Goldak, *et al.* (Refs. 12, 13), has achieved notable success in predicting the correct nugget shape and size using the cross-sectional model. This led to the hypothesis that the double ellipsoidal PDDF corresponded to the weld pool size and shape. Correct nugget shapes could not be predicted with flux or hemispherical heat source models with the cross-sectional kinematic model. In addition, the PDDF is computationally cheaper because it permits a coarser mesh than the flux model.

These considerations led to the interpretation of the PDDF as the residual in the heat equation when the temperature is prescribed.

Though the hemispherical heat source is expected to model an arc weld better than a disc source, it has its own limitations. The molten pool in many welds is far from spherical. Also, a hemispherical source is not appropriate for welds that are not spherically symmetric such as strip electrode, deep penetration electron beam or laser beam welds. These limitations can be overcome by using the appropriate power density distribution function such as the double ellipsoidal volume source (Ref. 3). Speed of the torch is also modeled in this. However, a hemispherical source, which is a special case of a double ellipsoidal PDDF, is used in this analysis.

Errors in the 2D Analysis

In order to estimate the error due to 2D approximation, first a 3D transient heat transfer analysis is carried out with a hemispherical heat source (Refs. 3, 4). Then a 2D heat transfer analysis is carried out for the equivalent mesh. The results of the 2D analysis are projected onto the 3D mesh and the two temperature fields are compared.

The difference is the error due to 2D approximation. In both 2D and 3D, Equation 1 was solved with the same PDDF.

The comparison can also be made in another way. First a 3D analysis was carried out in which Equation 1 is solved for temperature with the hemispherical PDDF. Then a 2D cross-sectional analysis is carried out in which the temperatures obtained from the 3D analysis are prescribed. In this 2D analysis, the temperatures are known and Equation 1 is solved for Q , the PDDF. This generates the reactions; i.e., thermal loads. These are the discrete form of the PDDF for the cross-sectional analysis. The two thermal loads can be compared; i.e., in the heat equation

$$\nabla \cdot k \nabla T + Q = C \frac{\partial T}{\partial t} \quad (7)$$

Table 1—Thermal Reactions Computed from 2-D Cross-Sectional Analysis with Prescribed Temperatures Obtained from 3-D Analysis

Node	Right Hand Side	Code	Output 1	Output 2	Output 3
	After		0.104 s	0.234 s	0.312 s
319		1	0.34433354 E-02	0.52516313 E+01	0.76409416 E+02
320		1	0.19022653 E+00	0.12708126 E-01	0.16918033 E-02
321		1	0.47750656 E+00	0.11053680 E+01	0.26195684 E+02
322		1	0.94466514 E-01	0.22739308 E+00	0.57582141 E+01
383		1	0.53703768 E+00	0.80262107 E+02	0.44768978 E+03
384		1	0.16693310 E+00	0.14763834 E+02	0.14106282 E+03
442		1	0.79797002 E+01	0.12509565 E+03	0.26934628 E+04
443		1	0.66333002 E-01	0.21242092 E+01	0.13882565 E+03
446		1	0.48611051 E+01	0.80002967 E+02	0.22644307 E+04
490		1	0.11143687 E+02	0.16476391 E+04	0.10773647 E+05
491		1	0.52315773 E-02	0.78862751 E+01	0.17494110 E+03
493		1	0.12346059 E-01	0.62618715 E+02	0.22250362 E+04
499		1	0.72218825 E+03	0.76931854 E+04	0.21313915 E+05
501		1	0.39759694 E+03	0.82471745 E+04	0.28870174 E+05
503		1	0.44637964 E-02	0.29516004 E+03	0.42452712 E+04
504		1	0.17289844 E-01	0.40280979 E-02	0.26711803 E+04
507		1	0.44757464 E-01	0.25811501 E+03	0.28084390 E+04
508		1	0.32259472 E-01	0.35610868 E+02	0.16638179 E+03
511		1	0.39766962 E+03	0.80035625 E+04	0.25611752 E+05
520		1	0.72221949 E+03	0.74939359 E+04	0.19323663 E+05
521		1	0.43487527 E+04	0.40413678 E+05	0.86323823 E+05
524		1	0.59290583 E+04	0.37953637 E+05	0.71872705 E+05
525		1	0.59290428 E+04	0.37878382 E+05	0.71512547 E+05
527		1	0.68086609 E+04	0.35151874 E+05	0.60891989 E+05
			Output 4	Output 5	Output 6
			0.528 s	1.716 s	2.808 s
Node		Code	Reactions due to prescribed variables		
319		1	0.13182560 E+03	0.10439605 E+03	0.51102572 E+03
320		1	0.19751869 E+02	0.31493231 E+02	0.97842749 E+03
321		1	0.51784025 E+02	0.10217206 E+03	0.43067569 E+03
322		1	0.61218378 E+01	0.27519070 E+02	0.80525617 E+02
383		1	0.10207559 E+04	0.23081596 E+03	0.23244088 E+04
384		1	0.38998974 E+03	0.26447156 E+03	0.18920345 E+04
442		1	0.13977449 E+05	0.18320574 E+05	0.26869535 E+05
443		1	0.27302116 E+04	0.59750142 E+04	0.12041619 E+05
446		1	0.15882182 E+05	0.23677970 E+05	0.38350721 E+05
490		1	0.33952989 E+05	0.33025102 E+05	0.39712396 E+05
491		1	0.29793666 E+04	0.51958879 E+04	0.88340542 E+04
493		1	0.12183680 E+05	0.15972103 E+05	0.23401976 E+05
499		1	0.49881641 E+05	0.36469607 E+05	0.35642780 E+05
501		1	0.71807651 E+05	0.58115095 E+05	0.60711855 E+05
503		1	0.16745321 E+05	0.19037708 E+05	0.25499882 E+05
504		1	0.36450267 E+04	0.57403392 E+04	0.90835693 E+04
507		1	0.99407135 E+04	0.11064109 E+05	0.14446647 E+05
508		1	0.21468954 E+04	0.32248117 E+04	0.50281865 E+04
511		1	0.61215900 E+05	0.47864463 E+05	0.48931197 E+05
520		1	0.43845547 E+05	0.30614711 E+05	0.29064536 E+05
521		1	0.19636875 E+06	0.10770650 E+06	0.85371396 E+05
524		1	0.18698563 E+06	0.77539909 E+05	0.54277346 E+05
525		1	0.18625807 E+06	0.77122820 E+05	0.53897735 E+05
527		1	0.22894046 E+06	0.59386721 E+05	0.36123291 E+05
			Output 7	Output 8	Output 9
			3.43 s	4.2 s	4.3 s
Node		Code	Reactions due to prescribed variables		
319		1	0.96824172 E-02	0.13075738 E-02	0.14071999 E-03
320		1	0.13957673 E+03	0.12625104 E+03	0.50323527 E+02
321		1	0.82753946 E-02	0.11381816 E-03	0.12394659 E-03
322		1	0.11496905 E+03	0.10068780 E+03	0.28417450 E+02
383		1	0.53912564 E+04	0.93836301 E+04	0.14257799 E+05
384		1	0.46796132 E+04	0.85653462 E+04	0.13339359 E+05
442		1	0.33455442 E+05	0.38142949 E+05	0.41532785 E+05
443		1	0.18624640 E+05	0.24938172 E+05	0.30558435 E+05
446		1	0.51599810 E+05	0.62815901 E+05	0.71948906 E+05
490		1	0.42900513 E+05	0.44023969 E+05	0.43987148 E+05
491		1	0.12061191 E+05	0.14627707 E+05	0.16502290 E+05
493		1	0.29194387 E+05	0.33367951 E+05	0.36129457 E+05
499		1	0.33531118 E+05	0.30678829 E+05	0.28079035 E+05
501		1	0.59234364 E+05	0.55954683 E+05	0.52437585 E+05
503		1	0.29591693 E+05	0.31935094 E+05	0.32990988 E+05
504		1	0.11756776 E+05	0.13658152 E+05	0.14836948 E+05

